Gas Transmission Northwest Compressor Station No. 12

Unit 12B Cost Effectiveness Calculation Update Based on Vendor Cost Quote

Based on recent discussions with DEQ, support documentation regarding SCR performance, and a cost quote for Station 12, Unit 12B, an updated cost effectiveness calculation spreadsheet follows. Notes regarding the analysis and changes from the 2020 submittal follow:

- Vendor cost quote is attached. In the two-week period between the February and March web meetings with DEQ, the vendor was able to provide a quote for one unit: 12B
- Changes to the previous submittal are highlighted in yellow in the Excel sheet / table below.
- Capital costs (including related costs in adjacent rows) were marginally increased based on
 the vendor quote. The vendor provided a cost range, and the upper end applies because
 "tempering air" system is needed to ensure the exhaust temperature at the catalyst inlet is less
 than the design maximum. For simple cycle turbines, higher exhaust temperature requires
 this system.
- Aqueous ammonia reagent cost updated based on vendor quote of hourly feed rate (i.e., 7.7 gallons per hour of 19% aqueous ammonia), assumed operating hours, and reagent cost of \$1.05 per gallon.
 - Aqueous ammonia cost per gallon from cost quote (attached) for delivery to site with 8,000 gallon tank. Fuel surcharge varies; costs provided (\$1.012 per gallon) rounded up to \$1.05 per gallon to include an estimate of fuel surcharge.
- Annual maintenance materials costs marginally increased based on vendor quote. (Note that additional review is continuing regarding potentially larger annual maintenance (labor) costs based on users' experience.)
- In response to DEQ questions, an IES memo documents examples of SCR NOx reduction performance for SCR application to natural gas transmission compressor drivers. That memo supports the assumption in the GTN 2020 four factor analysis that assumed 75% reduction (or even 70% reduction) for units 12A, 12B, 13C, and 13D.
- Updated cost-effectiveness value is \$12,676 per ton, assuming PSEL based on 8,760 operating hours. Additional examples assuming other operating hours or utilization:
 - Same as above with DEQ assumption of 90% control: \$10,563 per ton
 - 80% control: \$11,883 per ton
 - 75% control and 75% utilization: \$16,590 per ton
 - 75% control and future forecast of high-end utilization (42.5%): \$28,562 per ton

Table 2. Rolls Royce Avon Turbine (Unit 12B) SCR NOx Control Cost Effectiveness (100% utilization case).

| NOx Control Cost Effectiveness Estimate | <u> </u> | | | | |
|---|---|---|-------------|----------------|---|
| Engine Manufacturer | Cooper-Rolls | | | | |
| Engine Manufacturer Model No. | Avon | | | | |
| Unit ID | 12B | | | | |
| Fuel Used | Natural Gas | | | | Color Logand |
| Emissions Control | SCR | | | | Color Legend User Data / Information Input Cell |
| | NOx | | | | |
| Combustion Control Purpose Target Reduction | 75% | | | | "Cumulative" Cost Cell for Primary Categories Cost Effectiveness (\$ / ton) |
| Target Reduction | 75% | | | | Cost Ellectiveness (\$7 ton) |
| Engine Design Conditions | | | | | Comments |
| Power Output | 14300 | (hp) | | | Rated HP |
| Engine Exhaust Temperature | | (F) | | | optional input |
| Engine Exhaust Rate | | (lb/hr) | | | optional input |
| Gas Volume | | (dscfm) | | | optional input |
| Full Load Engine Exhaust Composition: | | | | | Comments |
| Oxygen (O ₂₎ | | (vol. %) | | | optional input |
| Carbon Dioxide (CO ₂₎ | | (vol. %) | | | optional input |
| Water (H ₂ O) | | (vol. %) | | | optional input |
| Oxides of Nitrogen (NOx) | | (ppmvd) | | | optional input |
| Nitrogen (N ₂) | | (vol. %) | | | optional input |
| NOx | 22.4 | l lb/hr | 0.470 | (lb/MMBtu) | NOx emissions from test Data: 173.9 lb/MMSCF ~0.170 lb/MMBt |
| NOX | ۷۵. | 1 10/111 | 0.170 | (ID/IVIIVIDIU) | NOX emissions from test data. 173.9 ib/MiNSCF ~0.170 ib/MiNBt |
| Engine Parameters | | | | | Comments |
| Total Operating Hours per Season | 8760 | (hrs) | 100.0% | utilization | |
| | | | | | |
| Final Exhaust Gas Composition Oxides of Nitrogen (NOx) | 5.0 | B lb/hr | 0.043 | (lb/MMBtu) | Comments Assume 75% reduction |
| | 5.0 | 10/11 | 0.043 | (ID/IVIIVIDIU) | |
| Economic Parameters | A 1 : | | | | Comments |
| Source of Cost Data | see Analysis | | | | Analysis primarily relying on EPA Cost Manual |
| Direct Costs | | Cost Formula | | | Comments |
| Combustion Control Equipment and Auxiliary | \$3,000,000 | | | | Updated per AeriNox proposal for SCR system hardware costs |
| Equipment | | (A) | | | (\$3,300,000); tempering air needed to ensure exhaust temperature < |
| Instrumentation | \$300,000 | (0.1*A) | | | |
| Sales Taxes | \$0 | (0.03*(A+instrun | nentation)) | | No Oregon sales tax |
| | | (0.05*A) | | | Updated per freight estimate in AeriNox proposal |
| Freight Purchased Equipment Cost (REC) | \$185,000 | | | | |
| Purchased Equipment Cost (PEC) | \$3,485,000 | PEC | | | |
| Purchased Equipment Cost (PEC) Direct Installation Costs | \$3,485,000 | PEC Cost Formula | | | Comments |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports | \$3,485,000 \$278,800 | PEC Cost Formula (0.08*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection | \$3,485,000 \$278,800 \$487,900 | PEC Cost Formula (0.08*PEC) (0.14*PEC) | | | Calculated Cost using EPA Control Cost Manual Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection Electrical | \$3,485,000 \$278,800 \$487,900 \$139,400 | PEC Cost Formula (0.08*PEC) (0.14*PEC) (0.04*PEC) | | | Calculated Cost using EPA Control Cost Manual Calculated Cost using EPA Control Cost Manual Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection Electrical Piping | \$3,485,000 \$278,800 \$487,900 \$139,400 \$69,700 | PEC Cost Formula (0.08*PEC) (0.14*PEC) (0.04*PEC) (0.02*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection Electrical Piping Insulation for ductwork | \$3,485,000 \$278,800 \$487,900 \$139,400 \$69,700 \$34,850 | PEC Cost Formula (0.08*PEC) (0.14*PEC) (0.04*PEC) (0.02*PEC) (0.01*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection Electrical Piping | \$3,485,000 \$278,800 \$487,900 \$139,400 \$69,700 \$34,850 \$34,850 | PEC Cost Formula (0.08*PEC) (0.14*PEC) (0.04*PEC) (0.02*PEC) (0.01*PEC) (0.01*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection Electrical Piping Insulation for ductwork | \$3,485,000 \$278,800 \$487,900 \$139,400 \$69,700 \$34,850 \$34,850 \$0 | PEC Cost Formula (0.08*PEC) (0.14*PEC) (0.04*PEC) (0.02*PEC) (0.01*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection Electrical Piping Insulation for ductwork Painting | \$3,485,000 \$278,800 \$487,900 \$139,400 \$69,700 \$34,850 \$34,850 | PEC Cost Formula (0.08*PEC) (0.14*PEC) (0.04*PEC) (0.02*PEC) (0.01*PEC) (0.01*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Purchased Equipment Cost (PEC) Direct Installation Costs Foundations and Supports Handling and Erection Electrical Piping Insulation for ductwork Painting Site Preparation | \$3,485,000 \$278,800 \$487,900 \$139,400 \$69,700 \$34,850 \$34,850 \$0 | PEC Cost Formula (0.08*PEC) (0.14*PEC) (0.04*PEC) (0.02*PEC) (0.01*PEC) (0.01*PEC) | | | Calculated Cost using EPA Control Cost Manual Cost included with next row |

Table 2 (continued).

| 7 Indirect Costs | | Cost Formula | | | Comments |
|--|----------------|----------------|------------|----------------|---|
| Engineering | \$348,500 | (0.10*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Construction and field expenses | \$174,250 | (0.05*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Contractor fees | \$348,500 | (0.10*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Start-up | \$69,700 | (0.02*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Performance test | \$34,850 | (0.01*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Contingencies | \$104,550 | (0.03*PEC) | | | Calculated Cost using EPA Control Cost Manual |
| Total Indirect Costs (IC) | \$1,080,350 | (0.31*PEC) | | | |
| 8 Capital Cost Summary | | | | | Comments |
| Total Direct Capital Costs (DC) | \$5,565,500 | | | | |
| Total Indirect Capital Costs (IC) | \$1,080,350 | | | | |
| Total Capital Investment (TCI) | \$6,645,850 | | | | |
| O Direct Assessed Contra | | 0 | | | , On-manufa |
| 9 Direct Annual Costs | #00.000 | Cost Formula | | | Comments |
| Operator Labor | \$26,000 | nominal cost | | | 5 hours per week (1 hr x 5 days); job category labor rate |
| Supervisor Labor | \$3,900 | | | | 15% of operator |
| Operating Materials - ammonia | \$70,825 | | | | materials estimates:7.7 gals aqueous NH3/hr at cost of \$1.05 / gallo |
| Maintenance - Labor | \$26,000 | nominal cost | | | 5 hours per week (1 hr x 5 days); job category labor rate |
| Maintenance - Materials | \$8,000 | nominal cost | | | Updated per AeriNOx quote for annual service parts |
| Catalyst maintenance / replacement | \$150,000 | | | | Engineering Estimate (5% of Cap Cost) |
| Testing and QA/QC | \$20,000 | | | | Engineering estimate - Annual test; reagent controller QA |
| Electricity | \$2,500 | | | | Estimate based on analysis in PA DEP TSD |
| Total Direct Annual Costs | \$307,225 | | | | |
| 10 Indirect Annual Costs | | Cost Formula | Capital Re | ecovery Factor | Comments |
| Overhead | \$38,340 | (0.6*(OL+SL+ML | .+MM)) | | |
| Administrative Charges | \$132,917 | (0.02*TCI) | ., | | Engine ACT Document |
| Property Taxes | \$66,459 | (0.01*TCI) | | | Engine ACT Document |
| Insurance | \$66,459 | (0.01*TCI) | | CRF | • |
| Capital Recovery | \$350,236 | CRF[TCI] | | 0.0527 | Factor for costs annualized over 30 years at 3.25% interest. |
| Total Indirect Annual Costs | \$654,410 | | | (| CRF = i * (1+i)^n / [(1+i)^n - 1] (i expressed as a decimal - e.g., 10% = 0 |
| 11 Summary | | | | | Comments |
| Total Direct Annual Operating Costs | \$307,225 | | | 1 | |
| Total Indirect Annual Operating Costs Total Indirect Annual Operating Costs | \$654,410 | | | | |
| Total Annual Costs | \$961,635 | | \$67 | 7 \$ per hp | |
| Incremental Annual Costs Over Baseline | \$961,635 | | ΨΟ7 | φροιτήν | |
| | . , | | | | _ |
| 12 Annual Emissions Reduction Over Baseline | | | | | Comments |
| Oxides of Nitrogen (NOx) | 75.87 | (Tons) | | | |
| | | | | | |
| Cost Effectiveness (\$/Ton) | | | | | Comments |